# TEST REPORT



REPORT NUMBER: 100719074PRT-004 REPORT DATE: July 3, 2012

### **EVALUATION CENTER**

Intertek Testing Services NA Inc. 22887 NE Townsend Way Fairview Oregon 97024

### **RENDERED TO**

Hearth & Home Technologies 1445 North Hwy Colville Washington 99114

### PRODUCT EVALUATED:

MODEL OEM LARGE PELLET FIRED ROOM HEATER

### PH50PS

Report of Testing Model OEM Large Pellet fired Room Heater for compliance as an "Affected Facility" with the applicable requirements of the following criteria: EPA Method 28 "Certification and Auditing of Wood Heaters" and EPA Method 5G "Determination of Particulate Matter Emissions from Wood Heaters".

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### I. INTRODUCTION

Intertek Testing Services NA (Intertek) has conducted testing for Hearth & Home Technologies, on model OEM Large Pellet Fired Solid Fuel Room Heater, to evaluate all applicable performance requirements included in EPA Method 28 "Certification and auditing of wood heaters" and Method 5G "Determination of particulate matter emissions from wood heaters." Method 5G2 was used to evaluate emission rates from the OEM Large Pellet stove. 5G2 utilizes a Method 5H sample train that extracts samples from a Dilution Tunnel. This method does not require results be corrected to obtain an EPA adjusted emission result.

### I.A PURPOSE OF TEST

The test was conducted to determine if the unit is in accordance with U.S EPA requirements under 40 CGR 60 SUBPART AAA, NSPS for Residential Wood Heaters. This evaluation was conducted on April 25, 2012

### I.B LABORATORY

The test on the OEM Large Pellet fired Solid Fuel Room Heater was conducted at the client facility located at 1445 North Highway, Colville Washington. The facility elevation is 1635 feet above sea level. Intertek Portland is accredited by the U.S. EPA, Certificate Number 8. The test was conducted by Bruce Davis.

### I.C DESCRIPTION OF UNIT

The model OEM Large Solid Fuel Room Heater is constructed of carbon steel. The outer dimensions are 24-inches deep, 34-inches high, and 24-inches wide. The unit has a door located on the front with a viewing glass for loading the fuel. Heat output is controlled via a control knob located on the right side of the appliance. Between minimum and maximum heat output settings is labeled as "Dynamic Mode". Within this mode are three individual heat output settings that the appliance will automatically modulate between in an attempt to maintain a predetermined temperature differential within the unit. Due to this modulation it was determined by the manufacturer that the appliance would not operate on its own within a medium low and medium high burn rate category as specified by the test method. An approval was granted by EPA representative John Dupree to allow the appliance to be held in one of the three Dynamic mode settings via a computer interface in order to conduct a medium low and medium high burn rate test.

(See product drawings.)

Proprietary drawings and manufacturing methods are on file at Intertek in Intertek's Portland, OR office.



Client Hearth & Home Technology Project No. G100719074

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### I.D REPORT ORGANIZATION

This report includes summaries of all data necessary to determine compliance with the regulations. Raw data, calibration records, intermediate calculations, drawings, specifications and other supporting information are contained in appendices to this report.

### II. SUMMARIZATION

### **II.A PRETEST INFORMATION**

A sample was submitted to Intertek directly from the client at the Hearth & Home test facility, the sample was not independently selected for testing. The test unit was received at the client facility on April 24, 2012. The unit was inspected upon receipt and found to be in good condition. The unit was set up following the manufacturer's instructions without difficulty.

Following assembly, the unit was placed on the test stand and instrumented with thermocouples in the specified locations. Prior to beginning the emissions tests the unit had been operated in excess of 10 hours during research and development tests conducted by Hearth & Home personnel.

Prior to testing the unit's chimney system and laboratory dilution tunnels was cleaned using standard wire brush chimney cleaning equipment.

### **II.B INFORMATION LOG**

### **TEST STANDARD**

From April 25 through April 26, 2012 the unit was tested for EPA emissions using test method 5G2. A sample train described in EPA method 5H was used to extract a proportionate sample from the dilution tunnel. A heated front filter, four Impingers and a rear filter made up the sample train.

### **Deviation from Standard Method**

No deviations from the standards were performed, however, only the applicable sections from each standard were used during all testing.

### **II.C SUMMARY OF TEST RESULTS**

RUN #1 April 25, 2012: Control knob was set to minimum output, feed rate, combustion blower, and convection fan automatically set to a predetermined setting via a printed circuit board. A burn rate of 0.62 kg/hr was achieved producing 9,256 BTU's per hour using EPA calculation.



RUN #2 April 25, 2012: Control knob was set to maximum output, feed rate, combustion blower, and convection fan automatically set to a predetermined setting via a printed circuit board. A burn rate of 2.17 kg/hr was achieved producing 32,396 BTU's per hour using EPA calculations.

RUN #3 April 26, 2012: Control knob on the appliance was set to maximum and the heat output was controlled via a computer interface (see stove description section I.C) Auger feed time set to 1.6 seconds on out of a 7 second duty cycle. Combustion blower was set to a program value of 2080. A burn rate of 0.98 kg/hr was achieved producing 14,640 BTU's per hour using EPA calculations.

RUN #4 April 26, 2012: Control knob on the appliance was set to maximum and the heat output was controlled via a computer interface (see stove description section I.C) Auger feed time set to 2.2 seconds on out of a 7 second duty cycle. Combustion blower was set to a program value of 2200. A burn rate of 1.36 kg/hr was achieved producing 20,303 BTU's per hour using EPA calculations.

### **II.D SUMMARY OF OTHER DATA**

### **EMISSIONS**

Run Number	Test Date	Burn Rate (kg/hr)	Emission Rate (g/hr)	Heating Efficiency* (% HHV)
1	4/25/12	2.17	1.12	84.4
2	4/25/12	0.62	0.59	85.2
3	4/26/12	0.98	0.76	84.9
4	4/26/12	1.36	0.60	84.4

<sup>\*</sup>Efficiency determined per CSA B415.1-2010.

### WEIGHTED AVERAGE CALCULATION

VVLI	WEIGHTED AVERAGE GALGGLATION								
Test No.	Burn Rate	tate		Probability	(K) Weighting Factor	(KxE)			
2	0.62	0.59	9,256	0.1084	0.3592	0.2119			
3	0.98	0.76	14,631	0.3592	0.5538	0.4209			
4	1.36	0.60	20,304	0.6622	0.5744	0.3446			
1	2.17	1.12	32,396	0.9336	0.3378	0.3783			
	Totals: 1.8252								
	Weighted average emission rate:								



### **TEST FACILITY CONDITIONS**

	/ tolair i oo itarii o ito								
		Room	Room	Baro.	Baro.	Air	Air		
Run	Temp.	Temp	Pres.	Pres.	Vel.	Vel.			
	un	°F	۰F	In. Hg	In. Hg	Ft/min	Ft/min		
		before	after	before	after	before	after		
	1	79	84	28.30	28.26	<50	<50		
	2	76	72	28.26	28.26	<50	<50		
	3	71	73	27.93	27.91	<50	<50		
	4	76	73	27.91	28.16	<50	<50		

### DILUTION TUNNEL FLOW RATE MEASUREMENTS AND SAMPLING DATA (5G-2)

Run No.	Burn	Velocity	Volumetric	Total	Volume	Particulate
	Time	(ft/sec)	Flow Rate	Temp.	of	Catch
NO.	(min)		(dscf/min)	(°R)	Sample	(mg)
1	120	13.46	135.32	561	62.763	8.66
2	120	12.42	129.20	542	62.415	4.76
3	120	14.17	146.38	539	62.905	5.46
4	120	12.35	126.34	547	61.562	4.85

### **GENERAL SUMMARY OF RESULTS**

	OLIVEI WILL GOMMIN (IV) OF IVEGOLIO								
Run No.	Burn Rate (kg/hr)	Change In Surface Temp (°F)	Initial Draft (in/H <sub>2</sub> O)	Run Time (min)	Average Draft (in/H <sub>2</sub> O)				
1	0.62	1.0	-0.042	120	-0.042				
2	2.17	8.2	-0.021	120	-0.02				
3	0.98	0.0	-0.028	120	-0.028				
4	1.36	21.2	-0.032	120	-0.032				

### III. PROCESS DESCRIPTION

### **III.A TEST SET-UP DESCRIPTON**

A standard 6" diameter single wall pipe and insulated chimney system was installed to 15' above floor level as specified by EPA regulations. A 3 inch elbow was installed at the flue collar; a 3" to 6" adaptor was installed directly to the top of the 3" elbow which connected to the 6" single wall pipe. A 3" pellet vent transition to 6" single wall pipe stove pipe is shown as an option in manufactures installation instruction in addition to standard 3" and 4" pellet vent pipe.

### **III.B AIR SUPPLY SYSTEM**

Combustion air enters through a tube located at the rear of the appliance. This



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tube is connected directly to the firebox and firepot. Air control is achieved by a programmed speed control of the combustion blower creating a vacuum to the air inlet tube.

### IV. SAMPLING SYSTEMS

### IV.A. SAMPLING LOCATIONS

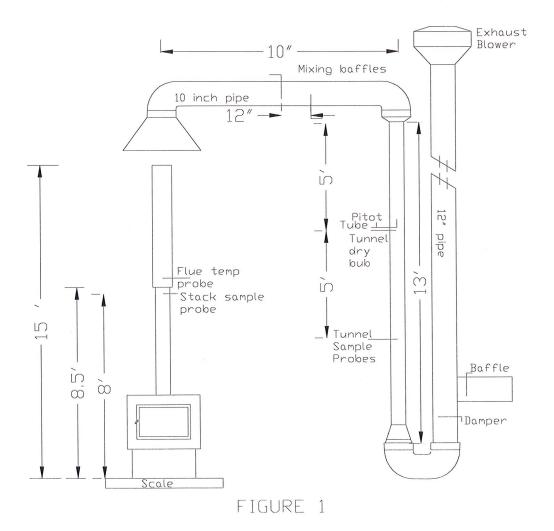
Particulate samples are collected from the vertical sample section of the dilution tunnel. The tunnel has two elbows and two mixing baffles in the system ahead of the sampling section. The sampling section is a continuous section of 6 inch diameter pipe straight over its entire length. Tunnel velocity pressure is determined by a standard Pitot tube located a minimum of 4 feet upstream of the sample location. The dry bulb thermocouple is located six inches downstream from the Pitot tube. Actual tunnel used was verified to meet EPA specifications and is similar to that shown in figure 1.

Stack gas samples are collected from the steel chimney section 8 feet  $\pm$  6 inches above the scale platform. Actual gas sample collection train was similar to that shown in figure 2.

An emissions sample train similar to that shown in figure 3 was used; a glass probe was used in place of a heated probe and button hook nozzle.

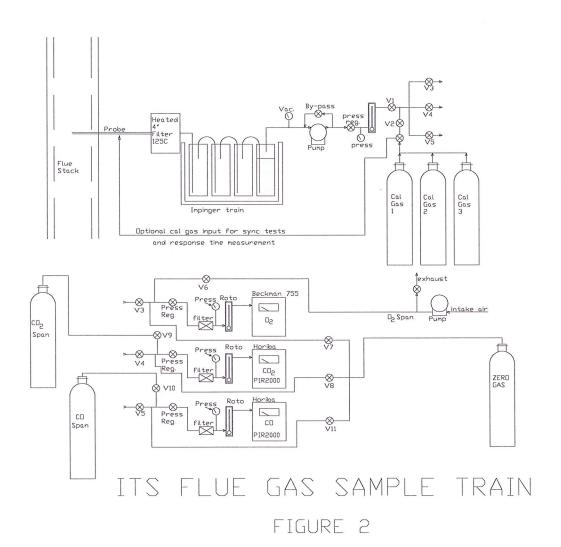


### IV.A.(1) DILUTION TUNNEL



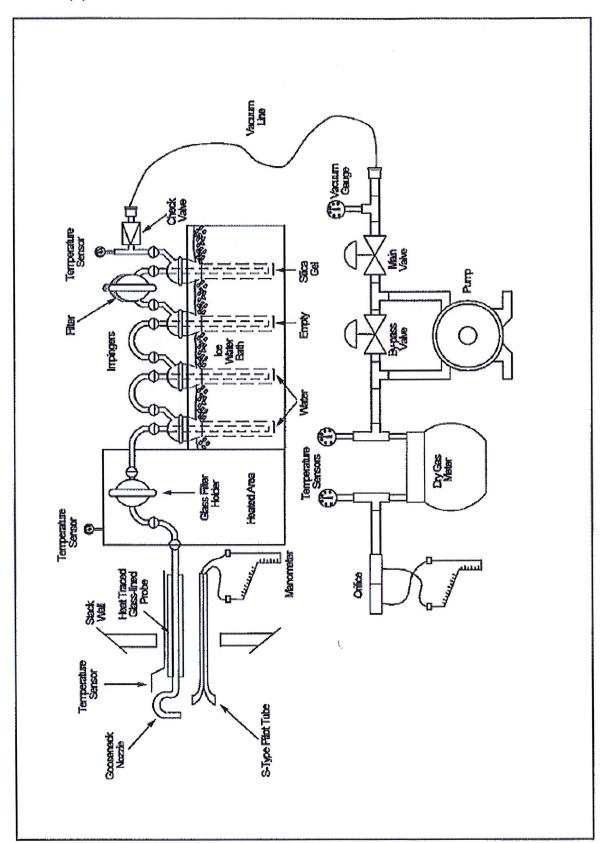
### **IV.B.OPERATIONAL DRAWINGS**

### IV.B.(1) STACK GAS SAMPLE TRAIN





IV.B.(2). DILUTION TUNNEL SAMPLE SYSTEMS





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### V. SAMPLING METHODS

### V.A. PARTICULATE SAMPLING

Particulates were sampled in strict accordance with EPA Method 5G-2 and 5H. A 5H sample train was used to extract particulate samples proportionally from a dilution tunnel. A glass probe was inserted into the tunnel and sample was drawn across a heated 110mm filter. After the heated front filter gasses entered a set of four Impingers, a rear 55mm filter was placed between number three and four Impingers. Sample analysis consisted of a front and back half acetone rinse. Impinger water was subjected to a Dichloromethane extraction to separate organics prior to oven drying.

### VI. QUALITY ASSURANCE

### VI.A. INSTRUMENT CALIBRATION

### VI.A. (1) DRY GAS METERS

At the conclusion of each test program the dry gas meters are checked against our standard dry gas meter. Three runs are made on each dry gas meter used during the test program. The average calibration factors obtained are then compared with the six-month calibration factor and, if within 5%, the six-month factor is used to calculate standard volumes. Results of this calibration are contained in Appendix D.

An integral part of the post test calibration procedure is a leak check of the pressure side by plugging the system exhaust and pressurizing the system to 10" W.C. The system is judged to be leak free if it retains the pressure for at least 10 minutes.

The standard dry gas meter is calibrated every 12 months using an accredited calibration agency. All calibration values are verified to be within EPA specifications.



### VI.A.(3). GAS ANALYZERS

The continuous analyzers are zeroed and spanned before each test with appropriate gases. A mid-scale multi-component calibration gas is then analyzed (values are recorded). At the conclusion of a test, the instruments are checked again with zero, span and calibration gases (values are recorded only). The drift in each meter is then calculated and must not exceed 5% of the scale used for the test.

At the conclusion of each unit test program, a five-point calibration check is made. This calibration check must meet accuracy requirements of the applicable standards. Consistent deviations between analyzer readings and calibration gas concentrations are used to correct data before computer processing. Data is also corrected for interferences as prescribed by the instrument manufacturer's instructions.

### **VI.B. TEST METHOD PROCEDURES**

### VI.B.(1). LEAK CHECK PROCEDURES

Before and after each test, each sample train is tested for leaks. Leakage rates are measured and must not exceed 0.02 CFM or 4% of the sampling rate. Leak checks are performed checking the entire sampling train, not just the dry gas meters. Pre-test and post-test leak checks are conducted with a vacuum of 10 inches of mercury. Vacuum is monitored during each test and the highest vacuum reached is then used for the post test vacuum value. If leakage limits are not met, the test run is rejected. During, these tests the vacuum was typically less than 2 inches of mercury. Thus, leakage rates reported are expected to be much higher than actual leakage during the tests.

### VI.B.(2). TUNNEL VELOCITY/FLOW MEASUREMENT

The tunnel velocity is calculated from a center point Pitot tube signal multiplied by an adjustment factor. This factor is determined by a traverse of the tunnel as prescribed in EPA Method 1. Final tunnel velocities and flow rates are calculated from EPA Method 2, Equation 6.9 and 6.10. (Tunnel cross sectional area is the average from both lines of traverse.)

Pitot tubes are cleaned before each test and leak checks are conducted after each test.

### VI.B.(3). PM SAMPLING PROPORTIONALITY (5G)

Proportionality was calculated in accordance with EPA Method 5G. The data and results are included in Appendix G.



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### VII. CONCLUSION

Results of this test show the OEM Large when operated following guidelines specified in EPA method 28 does meet emissions limits regulating an affected facility in the EPA New Source Performance Standards.

### VII.A RESULTS AND OBSERVATIONS

The Model OEM Large Pellet fired Solid Fuel Room Heater has been found to be in compliance with the applicable performance and construction requirements of the following criteria: EPA Method 28 "Certification and auditing of wood heaters" and Method 5G Determination of particulate matter emissions from wood heaters."

### INTERTEK TESTING SERVICES NA

Reported by:

Bruce S Davis

Test Engineer

Reviewed by:

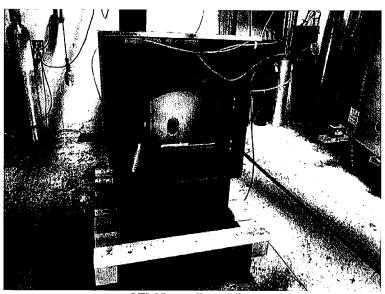
วัดhn Voorhees

**Operations Manager** 



# **Appendix F Test Data**

# Hearth & Home Technologies OEM Large Pellet G100719074



OEM Large Front View



V 1.1

# **EPA NSPS WEIGHTED AVERAGE CALCULATION**

Hearth & Home Client

**OEM Large** Model

4/25/2012 Date

PRT1204201552-002 G100719074 Sample Project

Stove: Weighted Average

2=noncat 1=cat

ന

Type of

3=pellet

0.00 0.00 30.60 47.02 48.48 0.00 0.00 0.00 **KXOHE** 28.51 0.3446 0.000.0 0.2119 0.000.0 0.4209 0.000.0 0.3783 0.000.0 0.000.0 (KXE) Weighting 0.5538 0.000.0 0.3592 0.5744 0.000.0 0.000.0 0.3378 0.000.0 0.0000 Factor Prob. 0.1084 1.0000 0.9336 1.0000 1.0000 1.0000 0.3592 0.6622 1.0000 0.00 0.00 9256.10 0.00 0.00 0.00 14630.62 32396.36 20303.71 (BTU/HR) Output Heat 84.90 85.20 84.40 84.40 (OHE) AHH 0.59 92.0 09.0 1.12 Rate g/hr Emission Ave. (E)0.62 0.98 1.36 2.17 Rate Burn 3 4 No. **Pest** 

1,0805 X 92.0 92.0 91.7 9101

HU Caleulakd

0.000.0 0.000.0

154.61 1.3558 1.8252 Totals:

0.7428 84.71 Weighted average emissions rate: Weighted Average OHE:



### TEST RESULTS EPA METHOD 5G-3

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 1

Dry Burn-Rate, kg/hr:						
Emission	n-Rate, g/hr:	1.12				
Duration of Test, Minutes	12	0				
Dry Gas Meter Standardization	Train A					
Dry Gas Meter Beginning Reading, ft <sup>3</sup> Dry Gas Meter Ending Reading, ft <sup>3</sup>	295.372 363.07					
Barometric Pressure Correction Factor Dry Gas Meter Calibration Factors (γ factors) Dry Gas Meter Temperature Factors Dry Gas Meter Delta-H Correction Factors	0.945 0.994 0.984 1.002					
Dry Gas Meter STD Volume Sampled, ft <sup>3</sup>	62.763					
Dillution Tunnel Flow / Volume	· · · · · · · · · · · · · · · · · · ·					
Standardized Tunnel Flow, dscfm	135.3	316				
Total Tunnel Volume, scf	16237	.967				
Emission Caclulations	Train A					
Sample Ratios (Total Tunnel Volume / Total Sample Volume) Sample Particulate Mass, mg Total Emissions, grams	258.719 8.7 2.240					
Emission-Rate, g/hr Adjusted Emission Rates, g/hr	1.12 <b>2.00</b>					
Operating Parameters	Train A					
Max Filter Temperature, °F Post-Test Leak Check, cfm @ in. Hg vac.	232 0.0@5"					
Average Firebox Surface Temperture delta-T, °F Maximum Ambient Temperture, °F Mimimum Ambient Temperature, °F	1 84 77	1				
Fuel Properties						
Wet Fuel Load Weight, Ib. Dry-Basis Fuel Load Moisture Content, % Wet-Basis Fuel Load Moisture Content, %	10. <i>i</i> 6.4 6.0	-8				

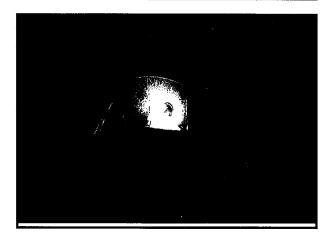
Test Engineer: 13 2

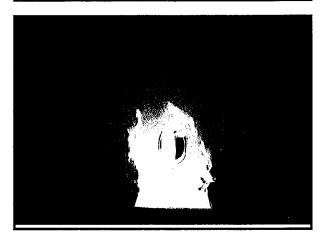


# Run Notes EPA Methods 28 and 5G-3

PROJECT / TEST INFORMATION					
Project Number:	G100719074				
Manufacturer:	Hearth N Home				
	OEM Large				
Sample ID Number:	PRT1204201552-001				
Test Date:	25-Apr-12				
Test Run Number:	1				
Date tunnel cleaned:	4/25/2012				
Purpose of Test	Cert High Burn				

Appliance Information						
Appliance Type:	3	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic				
Firebox Volume, ft <sup>3</sup> :	0	N/A for pellet type				
Convection Blower	3	1 - No Fan 2 - Fan Optional 3 - Fan Standard				





		Test Settings
Prim	ary Air:	NA
Second	lary Air:	NA
		Control set at maximum
Blow	er/Fan:	Automatic
		Pre- Burn Activities
Time Activ	vity	
Burr	ned at hi	igh for one hour
	-	
<u></u>		
		Start-Up Procedure
Loading of fue	l, sec. :	NA
Fuel-loading	g door :	NA
	nary air:	
	dary air:	
		Control set at maximum
Blowe	er / fan:	Automatic
		Other Notes
NA		

Test Engineer:

Date: 2-/-/2



# TEST FUEL DATA EPA METHOD 5G-3

Project Number: G100719074

Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 1

			-	 	
	Firebox \	/olume. f	<del>1</del> 3.	0	
			• •	•	

Calibration Reference ID		
Set meter to Species 1		
Set Temperature to 70F	12%	12.0
Set pin setting to 444	22%	22.0

	PRE-BURN FUEL PROPERTIES								
			L PROPE						
Eq. ID No.:		Time:		Temp.,°F:					
Piece No.	Length, In.	Weight, Lb.	Moisture, %, Dry Basis						
1									
2									
3									
4									
5									
6									
7									
8									
9									
10									
11									
12									
Total We	eiaht	0.0	Avera	iae. %db	#DIV/0!				

Allowable Fuel Load Range:

**0.0** to **0.0** 

TEST FUEL LOAD PROPERTIES								
Eq. ID No.:			Time:		Temp.,°F:			
Piece No.	Length,	Weigl	nt, Lb.	Moisture, %, Dry Basis				
1 1000 110.	ln.	2x4	4x4	111010	ta.o, 70, 21 <b>,</b>	340,0		
1		10.20		6.5	6.5	6.5		
2								
3								
4								
5								
6								
7								
8								
Total	S	10.2	0.0					
% of We	% of Weight 100		0					
Total weight	, wet, lb.	10	.20	Average M	loisture, dry	6.48		
			35 Average M		Noisture, wet 6.09			

Test Engineer: 802\_\_



Project Number: G100719074 Manufacturer:
Model:
Sample ID Number:
Test Date:

Model: 0EM Large
PRT1204201552-001
25-Apr-12

Test Run Number: 1

### **EPA Method 28** Pre Burn Data

Coal Bed Range 2.1 2.5

Average Firebox Temp, °F Final Coal Bed Wt, Ib 82.1

				Tem	oerature D	ata						
Duration, Minutes	Room	Dilution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Flue Draft	Fuel Weight	Weight Loss
0	68	81	205	489	351	319	432	401		-0.032	87.50	5.40
10	72	88	271	638	571	488	602	561		-0.04	86.50	1.00
20	73	90	279	651	587	500	615	574		-0.04	85.50	1.00
30	76	93	283	683	594	517	634	593		-0.04	84.50	1.00
40	77	95	283	665	592	516	628	587	•	-0.041	83.70	0.80
50	78	96	284	558	586	486	586	561		-0.042	83.00	0.70
60	78	96	280	655	572	503	610	576		-0.043	82.10	0.90
										,		
<b> </b>	<del></del>											
ļ												

Test Engineer:

Date: 7-/-/2



### **TEST DATA EPA METHOD 5G-3**

Project Number: G100719074

Manufacturer: Hearth N Home

Model: OEM Large

Sample ID No: PRT1204201552-001

Test Date: 25-Apr-12 Test Run No: 1

**Temperature Data** 

Firebox Temp Start Firebox Temp End 601.8 Firebox Delta-T

Max Filte	er Temps
Train A	
232	

Interval	10	Dura	tion of Tes	t, Min	120	İ'								
1	ime					Temperature Data								
Interval	Duration	Room	Dillution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Train A Filter	Impinger Exit	Train A DGM	
0	0	79	97	284	692	576	517	635	594		232	77	73	
1	10	77	98	285	689	584	516	632	589		231	45	73	
2	20	79	99	286	680	580	517	634	586		231	48	74	
3	30	81	100	288	684	582	521	630	587		230	55	75	
4	40	82	102	289	669	582	520	629	585		230	57	75	
5	50	79	101	284	674	557	496	612	571		230	61	76	
6	60	82	102	286	677	574	519	630	588		230	62	77	
7	70	80	102	288	686	581	527	637	595		231	64	78	
8	80	84	104	291	698	578	530	642	600		231	65	79	
9	90	80	102	289	695	579	527	638	598		230	65	78	
10	100	81	102	288	706	572	520	642	596		230	66	79	
11	110	81	102	282	683	543	498	618	579		232	66	78	
12	120	84	103	285	689	571	526	629	594		230	67	78	

Test Engineer:



### **TEST DATA EPA METHOD 5G-3**

### Gas Particulate Sampling Data

Project Number: G100719074 Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12 Test Run Number: 1

Barometer, In. Hg RI		RH, %	Sample	Box Correction (y	) Factors
Start	28.30		M	eter Box (A)	0.994
End	28.26				
Durati	on of Test	, Min	120		

Leak Check,	cfm @ in Hg
Train A	
0.0@5"	

Maximum	ı Vacuum
Train A	
0.00	

Durat	ion of Test	, Min	120						
	Particulate Sampling Data					The second secon			
Time	Tunnel Delta-P	Train A Delta-H		Flue Draft	Fuel Weight	Weight Loss	Train A Volume	Train A Proportional Rate	Train A Vacuum, In. Hg
0	0.040	1.00		-0.042	81.70	10.20	295.372	100.03	0.00
10	0.040	1.00	· · · · · · · · · · · · · · · · · · ·	-0.042	80.80	0.90	301.120	102.30	0.00
20	0.040	1.00		-0.042	79.90	0.90	307.000	104.55	0.00
30	0.040	1.00		-0.042	79.10	0.80	312.410	96.10	0.00
40	0.040	1.00		-0.042	78.30	0.80	317.750	95.03	0.00
50	0.040	1.00		-0.042	77.40	0.90	323.730	106.12	0.00
60	0.040	1.00		-0.042	76.60	0.80	329.110	95.38	0.00
70	0.040	1.00		-0.041	75.70	0.90	335.010	104.41	0.00
80	0.040	1.00		-0.041	74.90	0.80	340.280	93.25	0.00
90	0.040	1.00		-0.041	74.00	0.90	346.140	103.70	0.00
100	0.040	1.00		-0.041	73.20	0.80	351.750	99.09	0.00
110	0.040	1.00		-0.041	72.30	0.90	357.770	106.53	0.00
120	0.040	1.00		-0.041	71.50	0.80	363.070	93.87	0.00

Test Engineer:



# Dillution Tunnel Velocity Traverse EPA Method 5G-3

Initial Flow

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 1

	Dilution		
1	Delta P	Temp,°F	Square
	In. H2O	remp, r	Root
A1	0.0300	96	0.1732
A2	0.0360	96	0.1897
A3	0.0420	96	0.2049
A4	0.0360	96	0.1897
A Center	0.0400	96	0.2000
B1	0.0300	96	0.1732
B2	0.0400	96	0.2000
B3	0.0420	96	0.2049
B4	0.0360	96	0.1897
B Center	0.0400	96	0.2000
Averages	0.0372	96	0.1907

Tunnel Diameter	6.000	inches
Tunnel Static	-0.316	in. H2O
Tunnel Area	0.19635	Ft2
Pitot Correction	0.9534	factor
Baro. Pressure	28.30	
Pitot Factor	0.99	( 0.99 for standard, 0.84 or Cal. For S-Type )
Initial Velocity	13.391	Ft/ Sec

135.98 Ft3/min

Test Engineer:

Date: **7-/-**22



### **DILLUTION TUNNEL PARTICULATE CALCULATIONS** EPA Method 5G-3

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large
Sample ID Number: PRT1204201552-001
Test Date: 25-Apr-12

Test Run Number: 1

Intertek Equipment No.'s 19683, 19684

		FILTER #	WEIGHTS				
SAMPLE COMPONET	REAGENT	OR	FINAL, mg	TARE, mg	BLANK, mg/ml	PARTICULATE, mg	
FRONT FILTER CATCH	FILTER	392	713.9	710.9		3.00	
REAR FILTER CATCH	FILTER	402	165.6	165.8		-0.20	
RINSE OF PROBE &	ACETONE	45	99195.8			2.58	
RINSE OF IMPINGER SET	WATER	200	96379.9	96378.3	0	1.60	
RINSE OF IMPINGER SET	METHANE	100	109121.1	109120.5	0.002	0.40	
RINSE OF FILTER ASSEMBLY & GAS TRAIN -	ACETONE	40	95091	95089.7	0.0005	1.28	
					TOTAL:	8.66	

### **CONDENSED WATER**

		WEIGHTS						
IMPINGERS	FINAL, g	INITIAL, g	NET, g					
1	708.3	705.4	2.90					
2	701.8	691	10.80					
3	606.9	606.4	0.50					
4	999.3	990.4	8.90					
		TOTAL:	23.10					

### **EQUATIONS**

FRONT FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
REAR FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
RINSE OF PROBE & FILTER ASSEMBLY - FRONT	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF IMPINGER SET	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF FILTER ASSEMBLY & GAS TRAIN - BACK	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg

Fest Engineer:	Date:
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### **TEST RESULTS EPA METHOD 5G-3**

Project Number: G100719074 Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001 Test Date: 25-Apr-12

Test Run Number: 2

	Rate, kg/hr:	0.62				
Emission-Rate, g/hr:						
Duration of Test, Minutes	120	0				
ry Gas Meter Standardization	Train A					
Dry Gas Meter Beginning Reading, ft <sup>3</sup>	363.3					
Dry Gas Meter Ending Reading, ft <sup>3</sup>	430.583					
Barometric Pressure Correction Factor	0.945					
Dry Gas Meter Calibration Factors (γ factors)	0.994					
Dry Gas Meter Temperature Factors	0.986					
Dry Gas Meter Delta-H Correction Factors	1.002					
Dry Gas Meter STD Volume Sampled, ft <sup>3</sup>	62.415					
illution Tunnel Flow / Volume						
Standardized Tunnel Flow, dscfm	129.2	200				
Total Tunnel Volume, scf	15504	.016				
mission Caclulations	Train A					
Sample Ratios (Total Tunnel Volume / Total Sample Volume)	248.403					
Sample Particulate Mass, mg	4.8					
Total Emissions, grams	1.181					
Emission-Rate, g/hr	0.59					
Adjusted Emission Rates, g/hr	1.18					
perating Parameters	Train A					
Max Filter Temperature, °F	234					
Post-Test Leak Check, cfm @ in. Hg vac.	.005@5					
Average Firebox Surface Temperture delta-T, °F	8.2	2				
Maximum Ambient Temperture, °F	76					
Mimimum Ambient Temperature, °F	72	<u> </u>				
uel Properties		^				
Wet Fuel Load Weight, lb.	2.9					
Dry-Basis Fuel Load Moisture Content, %	6.4					
Wet-Basis Fuel Load Moisture Content, %	6.0	9				

Test Engineer:

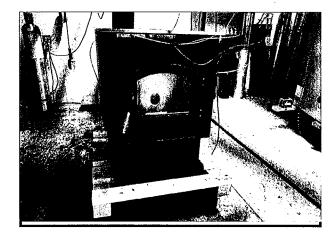
Date: 7-/-12

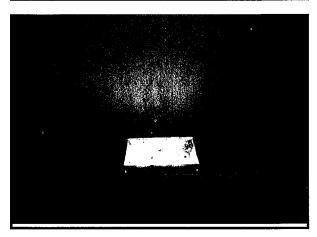


### Run Notes EPA Methods 28 and 5G-3

PROJECT / TEST INFORMATION					
Project Number:	G100719074				
Manufacturer:	Hearth N Home				
	OEM Large				
Sample ID Number:	PRT1204201552-001				
Test Date:	25-Apr-12				
Test Run Number:	2				
Date tunnel cleaned:	4/25/2012				
Purpose of Test	Certification				

Appliance Information							
Appliance Type:	3	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic					
Firebox Volume, ft <sup>3</sup> :	0	N/A for pellet type					
Convection Blower	3	1 - No Fan 2 - Fan Optional 3 - Fan Standard					





Test Settings								
Primary Air: NA								
Secondary Air: NA								
Control Board: Control set at minimum setting								
Blower/Fan: Automatic								
Pre- Burn Activities								
Time Activity								
No activity during pre burn								
Start-Up Procedure								
Loading of fuel, sec.: NA								
Fuel-loading door: NA								
Primary air: NA								
Secondary air: NA								
Control board: Set at minimum setting								
Blower / fan: Automatic								
Other Notes								
NA								

Test Engineer: 3/2=



# TEST FUEL DATA EPA METHOD 5G-3

Project Number: G100719074

Manufacturer: Hearth N Home
OEM Large
Sample ID Number: PRT1204201552-001
Test Date: 25-Apr-12

Test Run Number: 2

Firebox Volume, ft<sup>3</sup>: 0

Calibration Reference ID		
Set meter to Species 1		
Set Temperature to 70F	12%	12.0
Set pin setting to 444	22%	22.0

	PRE-BURN FUEL PROPERTIES									
Eq. ID No.:		Time:	Temp.,°F:							
Piece No.	Length, In.	Weight, Lb.	Moisture, %, Dry Basis							
1										
2										
3										
4										
5										
6										
7										
8										
9										
10										
11										
12										
Total We	eiaht	0.0	Avera	ige, %db	#DIV/0!					

Allowable Fuel Load Range: 0.0

	TEST FUEL LOAD PROPERTIES							
Eq. ID No.:			Time:		Temp.,°F:			
Piece No.	Length,	Weight, Lb.		Moisture, %, Dry Basis				
1 1000 140.	ln.	2x4	4x4	l Wors	itale, 70, Diy	Dasis		
1		2.90		6.5	6.5	6.5		
2								
3								
4								
5								
6								
7								
8			·	1				
Total	s	2.9	0.0					
% of We	eight	100	0					
Total weight	, wet, lb.	2.90		Average Moisture, dry		6.48		
Total weight	, dry, kg	1.24		Average Moisture, wet 6		6.09		

to

0.0

Test Engineer:

Date: 7-/-12



Project Number: G100719074 Manufacturer:
Model:
Sample ID Number:
Test Date:

Model: PRT1204201552-001
25-Apr-12

Test Run Number: 2

### **EPA Method 28** Pre Burn Data

Coal Bed Range

Final Coal Bed Wt, lb 68.9

Average Firebox Temp, °F 304.4

				Temp	perature D	ata	,		e politico e construir de		• • • • • • • • • • • • • • • • • • • •	
Duration, Minutes	Room	Dilution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Flue Draft	Fuel Weight	Weight Loss
0	78	90	191	339	346	261	325	309		-0.027	70.30	1.40
10	78	87	163	321	331	238	307	295		-0.022	70.10	0.20
20	75	84	157	316	335	233	301	290		-0.02	69.90	0.20
30	75	84	153	330	333	233	306	295		-0.02	69.70	0.20
40	75	83	154	331	339	239	312	298		-0.02	69.40	0.30
50	74	82	154	317	337	235	304	291		-0.021	69.20	0.20
60	76	85	176	333	334	248	311	296		-0.021	68.90	0.30
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Test Engineer: 802 -

Date: 7-/-12



### TEST DATA EPA METHOD 5G-3

**Temperature Data** 

Firebox Temp Start 303
Firebox Temp End 294.8
Firebox Delta-T 8.2

Max Filte	er Temps
Train A	
234	

Interval	10	Dura	tion of Tes	t, Min	120	· '	<del> </del>		*************			1		
Time					Temperature Data									
Interval	Duration	Room	Dillution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Train A Filter	Impinger Exit	Train A DGM	
0	0	76	85	175	328	331	248	312	296	,	233	75	76	
1	10	73	81	154	307	326	231	297	286		234	42	76	
2	20	72	81	152	324	335	236	308	296		233	42	76	
3	30	73	82	153	328	333	235	306	296		233	43	75	
4	40	74	82	152	326	330	233	306	295		233	44	75	
5	50	72	81	152	330	342	238	311	300		234	46	76	
6	60	75	83	167	318	317	326	241	307		234	47	76	
7	70	74	81	150	299	329	230	294	282		233	48	76	
8	80	74	82	151	308	331	231	299	287		233	48	76	
9	90	74	81	149	301	330	230	296	285		233	49	76	
10	100	76	82	149	297	330	227	293	282		234	50	76	
11	110	73	80	149	319	331	233	306	293		233	50	75	
12	120	72	82	167	320	321	240	305	288		234	51	75	

Test Engineer: B



### TEST DATA EPA METHOD 5G-3

### **Gas Particulate Sampling Data**

Project Number: G100719074

Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 2

Baromete	er, In. Hg	RH, %	Sample	Box Corr	ection (γ)	Factors		Leak Check, o	cfm @ in Hg	Maximum	i Vacuum
Start	28.26		М	eter Box (	A)	0.994		Train A		Train A	
End	28.26							<u>.005@5</u>		0.00	
Durati	on of Test	, Min	120				•	····			
							Particulate	Sampling Data			
									Train A	Train A	
i	Tunnel	Train A		Flue	Fuel	Weight	Train A		Proportional	Vacuum, In.	
Time	Delta-P	Delta-H		Draft	Weight	Loss	Volume		Rate	Hg	
0	0.038	1.00		-0.021	68.90	2.90	363.300		99.97	 0.00	
10	0.038	1.00		-0.021	68.60	0.30	368.950		100.63	0.00	
20	0.038	1.00		-0.021	68.40	0.20	374.570		100.10	0.00	
30	0.038	1.00		-0.020	68.20	0.20	380.000		96.99	0.00	
40	0.038	1.00		-0.020	67.90	0.30	385.580		99.67	0.00	
50	0.038	1.00		-0.020	67.70	0.20	391.170		99.57	0.00	
60	0.038	1.00		-0.020	67.40	0.30	396.850		101.36	0.00	
70	0.038	1.00		-0.020	67.20	0.20	402.750		105.09	0.00	
80	0.038	1.00		-0.020	66.90	0.30	407.970		93.06	0.00	
90	0.038	1.00		-0.021	66.70	0.20	413.630		100.81	0.00	- "
100	0.038	1.00		-0.021	66.50	0.20	419.330		101.62	0.00	.,_
110	0.038	1.00		-0.020	66.30	0.20	424.940		100.02	0.00	
120	0.038	1.00		-0.020	66.00	0.30	430.583		100.79	0.00	

Test Engineer: 3



# Dillution Tunnel Velocity Traverse EPA Method 5G-3

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 2

	Dilution	Tunnel		Tunnel D
1	Delta P	Temp,°F	Square	
	In. H2O	remp, r	Root	Tunnel S
A1	0.0280	83	0.1673	
A2	0.0400	83	0.2000	Tunnel A
A3	0.0400	83	0.2000	
A4	0.0360	83	0.1897	Pitot Cor
A Center	0.0420	83	0.2049	
B1	0.0260	83	0.1612	Baro. Pro
B2	0.0340	83	0.1844	
В3	0.0400	83	0.2000	Pitot Fac
B4	0.0340	83	0.1844	
B Center	0.0400	83	0.2000	Initial Ve
Averages	0.036	83	0.1859	

Tunnel Diameter	6.000	inches
Tunnel Static	-0.320	in. H2O
Tunnel Area	0.19635	Ft2
Pitot Correction	0.9181	factor
Baro. Pressure	28.26	
Pitot Factor	0.99	( 0.99 for standard, 0.84 or Cal. For S-Type )
Initial Velocity	12.911	Ft/ Sec
Initial Flow	134.05	Ft3/min

Test Engineer: 3



### **DILLUTION TUNNEL PARTICULATE CALCULATIONS** EPA Method 5G-3

Project Number: G100719074

Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 25-Apr-12

Test Run Number: 2

Intertek Equipment No.'s 19683, 19684, 19726

		FILTER # OR			WEIGHTS	
SAMPLE COMPONET	REAGENT	VOLUME, mi	FINAL, mg	TARE, mg	BLANK, mg/ml	PARTICULATE, mg
FRONT FILTER CATCH	FILTER	393	710.8	711.3		-0.50
REAR FILTER CATCH	FILTER	403	165.3	165.5		-0.20
RINSE OF PROBE &	ACETONE	35	96392.4	96390.6	0.0005	1.78
RINSE OF IMPINGER SET	WATER	205	104981.5	104981.2	0	0.30
RINSE OF IMPINGER SET	METHANE	100	98761.7	98762	0.002	0.00
RINSE OF FILTER ASSEMBLY & GAS TRAIN -	ACETONE	55	106097.8	106094.4	0.0005	3.37
					TOTAL:	4.76

### **CONDENSED WATER**

		WEIGHTS						
IMPINGERS	FINAL, g	INITIAL, g	NET, g					
1 """	708.2	706.3	1.90					
2	696.7	690.8	5.90					
3	606.2	605.4	0.80					
4	991.4	978.6	12.80					
		TOTAL:	21.40					

### **EQUATIONS**

FRONT FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
REAR FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
RINSE OF PROBE & FILTER ASSEMBLY - FRONT	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF IMPINGER SET	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF FILTER ASSEMBLY & GAS TRAIN - BACK	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg

Test Engineer: 3



### Supplemental Data EPA 5G/5H

Client: Hearth N Home

Model: OFm L Project #: G100719074 Sample ID #: PRT 1204201552-001

Date: 4/25/12

Run #: \_\_\_\_\_\_\_

Start Time: 16:15 Stop Time: 18:15

Intertek Equipment #'s: ETC5-4, ETC-11, ETC7-1

Gas Analyzer Train Leak Check:

Stack:

Dilution Tunnel (Method 5G Only):

Initial: 900 d

Final: 900 d

Final: 900 d

Final: \_\_\_\_

Span Gas CO<sub>2</sub>: 9.90 O<sub>2</sub>: \_\_\_\_

CO: 999 CO<sub>2</sub>(DT): \_\_\_\_

Calibrations:

	N <sub>2</sub> S	pan	N <sub>2</sub> S	Span	N₂ Span	N₂ Span	N₂ Span	N₂ Span	N <sub>2</sub> Span
Time	Q	グ	Ę	ンケ	J.				
O <sub>2</sub>									
CO <sub>2</sub>	0.00	10:00	-0.09	1994					
CO .	0.06	0.98	0.00	0.97					
CO <sub>2</sub> (DT)	M	1	·						

Stack Diameter (inches): 3 to 6"

Air Velocity (ft/min):

Scale Audit (lbs):

Initial: <u>450</u> Final: <u>450</u>

Pretest: <u>In.o.</u> Post Test: <u>In.o.</u>

Induced Draft: 00 %Smoke Capture: 100 Yo

Pitot Tube Leak Test: Pre: 00

Post: \_0.0\_

Flue Pipe Cleaned Prior to First Test in Series: Date: 4/25/14

Initials: <u>ろく</u>

	Initial	Middle	Ending
Pb (in/Hg)	28.26		28.26
Room Temp (°F)	76		72

Date: 7-/-/2
Engineer signature: 03



**Analytical Test Report** 

Twin Ports Testing, Inc. 1301 North 3rd Street Superior, WI 54880 p: 715-392-7114

p: 800-373-2562 f: 715-392-7163 www.twinportstesting.com

Report No:

USR:W212-0482-01

Issue No:

Signed:

This report replaces all previous issues

Client:

**HEARTH & HOME TECHNOLOGIES** 

1915 W Saunders St

Mount Pleasant

lΑ

52641

Attention:

Colin McCormick

PO No:

Amanda Sayles Chemistry Lab Technician

Date of Issue:

4/26/2012

amanda Saylis

THIS DOCUMENT SHALL NOT BE REPRODUCED EXCEPT IN FULL

Sample Details

Sample Log No:

Sample Designation:

W212-0482-01

Gallon sized pellet sample

Sample Recognized As: Pellets

Dallott sized pellet

Sample Time: Arrival Date:

Sample Date:

4/16/2012

**Test Results** 

	METHOD	UNITS	MOISTURE	AS
NA - i - 4 - 1			FREE	RECEIVED
Moisture Total	ASTM E871	wt. %		6.48
Ash	ASTM D1102	wt. %	0.26	0.24
Volatile Matter	ASTM D3175	wt. %		
Eixed Carbon by Difference	ASTM D3175	wt. %		
alfur	ASTM D4239	wt. %	0.030	0.028
SO <sub>2</sub>	Calculated	lb/mmbtu		0.065
Net Cal. Value at Const. Pressure	ISO 1928	GJ/tonne	19.24	17.84
Net Cal. Value at Const. Pressure	ISO 1928	J/g	19243	17839
Gross Cal. Value at Const. Vol.	ASTM E711	J/g	20581	19190
Gross Cal. Value at Const. Vol.	ASTM E711	Btu/lb	8849	8251
Carban	A OTM DECTO	. 0/	77.00	
Carbon	ASTM D5373	wt. %	50.33	46.93
Hydrogen	ASTM D5373	wt. %	6.15	5.73
Nitrogen	ASTM D5373	wt. %	< 0.20	< 0.19
Oxygen	ASTM D3176	wt. %	> 43.04	> 40.41
Chlorine	ASTM D6721	mg/kg		
Fluorine	ASTM D3761	mg/kg		
Mercury	ASTM D6722	mg/kg		
Bulk Density	ASTM E873	lbs/ft <sup>3</sup>		
Fines (Less than 1/8")	TPT CH-P-06	wt.%		
Durability Index	Kansas State	PDI		
Sample Above 1.50"	TPT CH-P-06	wt.%		
Maximum Length (Single Pellet)	TPT CH-P-06	inch		
Diameter, Range	TPT CH-P-05	inch		to
Diameter, Average	TPT CH-P-05	inch		7-
Stated Bag Weight	TPT CH-P-01	lbs		
Actual Bag Weight	TPT CH-P-01	lbs		

**omments** 



### TEST RESULTS EPA METHOD 5G-3

Project Number: G100719074 Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12
Test Run Number: 3

Dry Burn-	Rate, kg/hr:	0.98
Emission	n-Rate, g/hr:	0.76
Duration of Test, Minutes	12	0
Dry Gas Meter Standardization	Train A	
Dry Gas Meter Beginning Reading, ft <sup>3</sup> Dry Gas Meter Ending Reading, ft <sup>3</sup>	430.7 498.687	
Barometric Pressure Correction Factor Dry Gas Meter Calibration Factors (γ factors) Dry Gas Meter Temperature Factors Dry Gas Meter Delta-H Correction Factors	0.933 0.994 0.995 1.002	
Dry Gas Meter STD Volume Sampled, ft <sup>3</sup>	62.905	
Dillution Tunnel Flow / Volume		
Standardized Tunnel Flow, dscfm Total Tunnel Volume, scf	146. 17565	
mission Caclulations	Train A	,,,,,,
Sample Ratios (Total Tunnel Volume / Total Sample Volume) Sample Particulate Mass, mg Total Emissions, grams	279.235 5.5 1.524	
Emission-Rate, g/hr Adjusted Emission Rates, g/hr	0.76 <b>1.45</b>	
Operating Parameters	Train A	
Max Filter Temperature, °F Post-Test Leak Check, cfm @ in. Hg vac.	235 0.0 @ 8	
Average Firebox Surface Temperture delta-T, °F Maximum Ambient Temperture, °F Mimimum Ambient Temperature, °F	0 7 6	7
uel Properties		20
Wet Fuel Load Weight, Ib. Dry-Basis Fuel Load Moisture Content, % Wet-Basis Fuel Load Moisture Content, %	4.6 6.4 6.0	18

Test Engineer: 43/2

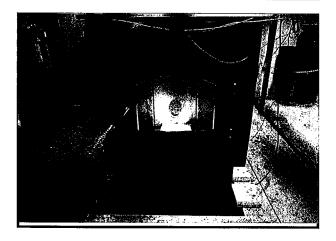
Date: 7-/-12

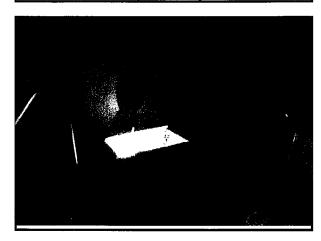


### Run Notes EPA Methods 28 and 5G-3

PROJECT / TEST INFORMATION								
Project Number:	G100719074							
Manufacturer:	Hearth N Home							
	OEM Large							
Sample ID Number:	PRT1204201552-001							
Test Date:	26-Apr-12							
Test Run Number:	3							
Date tunnel cleaned:	4/25/2012							
Purpose of Test	Certification							

Appliance Information									
Appliance Type:	3	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic							
Firebox Volume, ft <sup>3</sup> :	0	N/A for pellet type							
Convection Blower	3	1 - No Fan 2 - Fan Optional 3 - Fan Standard							





		Test Settings
	Primary Air:	NA
S	econdary Air:	NA
C	ontrol Board:	Power level two
	Blower/Fan:	Automatic
		Pre- Burn Activities
Time	Activity	
	No activity w	as noted
		Start-Up Procedure
	of fuel, sec. :	
Fuel-I	oading door :	
	Primary air:	
	econdary air:	
	ontrol board:	Computer input to hold constant burn rate
	Blower / fan:	
		Other Notes
Feed time	is 1.6 second	ds on out of 7 second duty cycle. Combustion blower at 2080

Test Engineer: 8/2-



Project Number: G100719074 Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001 Test Date: 26-Apr-12

Test Run Number:

Firebox Volume, f	ft <sup>3</sup> :	0

Calibration Reference ID		
Set meter to Species 1		
Set Temperature to 70F	12%	12.0
Set pin setting to 444	22%	22.0

	PRE-BURN FUEL PROPERTIES												
Eq. ID No.:		Time:		Temp.,°F:									
Piece No.	Length, In.	Weight, Lb.	Moi	Moisture, %, Dry Basis									
1					,								
2													
3													
4													
5													
6													
7													
8													
9													
10													
11													
12													
Total We	eight	0.0	0.0 Average, %db #DIV/0!										

Allowable Fuel Load Range:

0.0 to 0.0

TEST FUEL LOAD PROPERTIES  Eq. ID No.: Time: Temp., °F:												
Eq. ID No.:			Time:									
Piece No.	Length, In.	Weigl 2x4	Weight, Lb. Moisture, %, D		ture, %, Dry E	Basis						
1	111.	4.60	4x4	6.5	6.5	6.5						
2					0.0							
3												
4												
5												
6												
7												
8												
Total	s	4.6	0.0									
% of We	eight	100	0									
Total weight	, wet, lb.	4.	60	Average Moisture, dry 6.48								
Total weight	t, dry, kg	1.	96	Average M	oisture, wet	6.09						

Test Engineer:



Project Number:

Manufacturer:

Model:

Sample ID Number:

Test Date:

Test Run Number:

G100719074

Hearth N Home

OEM Large
PRT1204201552-001

26-Apr-12

3

### EPA Method 28 Pre Burn Data

Coal Bed Range 1.0 to 1.1

Average Firebox Temp, °F 379.4

Final Coal Bed Wt, lb 61.8

	Temperature Data											
Duration,		Dilution		Firebox	Firebox	Firebox	Firebox	Firebox	Catalyst	Flue	Fuel	Weight
Minutes	Room	Tunnel	Flue Gas	Тор	Bottom	Back	Left	Right	Outlet	Draft	Weight	Loss
0	68	73	172	425	434	298	392	378		-0.028	64.50	2.70
10	72	76	178	415	435	301	393	379		-0.028	64.20	0.30
20	69	74	178	418	437	304	401	384		-0.028	63.70	0.50
30	70	76	186	444	434	316	415	393		-0.028	63.30	0.40
40	70	77	186	422	426	313	402	387		-0.028	62.90	0.40
50	70	77	185	434	429	310	407	389		-0.028	62.60	0.30
60	69	78	185	418	426	306	399	382		-0.028	62.20	0.40
70	70	78	183	411	417	302	391	376		-0.028	61.80	0.40
	**************************************	· · · · · · · · · · · · · · · · · · ·										
	4						***************************************					
										L		

Test Engineer: 802 -

Date: 7-/-12



Project Number:

Manufacturer:

Model:

Sample ID No:

Test Date:

Test Run No:

PG100719074

Hearth N Home

OEM Large

PRT1204201552-001

26-Apr-12

3

**Temperature Data** 

Firebox Temp Start 388.2
Firebox Temp End 388.2
Firebox Delta-T 0.0

Max Filter Temps								
Train A								
235								

								Dona	0.0		200			
nterval	10	Dura	tion of Tes	t, Min	120	L '				•				
Ţ	Time			Temperature Data										
Interval	Duration	Room	Dillution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Train A Filter	Impinger exit	Train A DGM	
0	0	71	78	184	433	417	304	402	385		234	74	69	
1	10	72	80	185	421	421	304	396	381	***************************************	233	43	70	
2	20	70	79	187	400	394	296	386	365		233	44	70	
3	30	77	79	183	411	405	300	395	376		233	48	70	
4	40	70	78	183	417	407	303	395	380		234	50	71	
5	50	71	79	184	404	411	299	391	375		232	51	71	
6	60	69	79	182	410	408	298	387	372		233	53	71	
7	70	70	79	184	442	415	310	407	390		234	54	71	
8	80	73	81	192	392	406	303	381	364		235	55	71	
9	90	73	81	185	410	401	298	384	370		234	56	71	
10	100	69	78	182	421	405	299	392	378		233	54	71	
11	110	72	80	183	396	408	300	387	370		234	54	71	1
12	120	73	80	186	427	411	310	407	386		234	55	71	

Test Engineer: 3/2



### Gas Particulate Sampling Data

Project Number: G100719074

Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 3

0.048

1.00

Baromete	er, In. Hg	RH, %	Sample	Box Corr	ection (γ)	Factors		Leak Check,	cfm @ in Hg		Maximum	i Vacuum
Start	27.93		M	eter Box (	(A)	0.994		Train A			Train A	
End	27.91							0.0 @ 8			0.00	
Durati	on of Test	, Min	120							·		
***************************************	Particulate Sampling Data											
Time	Tunnel Delta-P	Train A Delta-H		Flue Draft	Fuel Weight	Weight Loss	Train A Volume		Train A Proportional Rate		Train A Vacuum, In. Hg	
0	0.048	1.00		-0.028	61.70	4.60	430.700		100.01		0.00	
10	0.048	1.00		-0.028	61.30	0.40	436.370		100.28		0.00	
20	0.048	1.00		-0.030	60.90	0.40	442.330		105.31		0.00	
30	0.048	1.00		-0.029	60.50	0.40	447.950		99.31		0.00	
40	0.048	1.00		-0.028	60.20	0.30	453.480		97.44		0.00	
50	0.048	1.00		-0.028	59.70	0.50	459.060		98.41		0.00	
60	0.048	1.00		-0.028	59.40	0.30	464.680		99.12		0.00	
70	0.048	1.00		-0.028	59.00	0.40	470.350		100.00		0.00	
80	0.048	1.00		-0.028	58.60	0.40	476.050		100.72	-	0.00	
90	0.048	1.00		-0.028	58.30	0.30	481.630		98.60		0.00	
100	0.048	1.00		-0.028	57.90	0.40	487.330		100.44		0.00	
110	0.048	1.00		-0.028	57.50	0.40	493.060		101.15		0.00	
											0.00	

498.687

-0.028 57.10

Test Engineer:

Date: 7-1-12

0.00



# Dillution Tunnel Velocity Traverse EPA Method 5G-3

Initial Flow

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 3

	Dilution			
	Delta P	Temp,°F	Square	
	In. H2O		Root	
A1	0.0360	79	0.1897	
A2	0.0440	79	0.2098	
A3	0.0440	79	0.2098	
A4	0.0420	79	0.2049	
A Center	0.0480	79	0.2191	
B1	0.0360	79	0.1897	
B2	0.0420	79	0.2049	
B3	0.0460	79	0.2145	
В4	0.0420	79	0.2049	
B Center	0.0480	79	0.2191	
Averages	0.0428	79	0.2035	

Tunnel Diameter	6.000	inches
Tunnel Static	-0.300	in. H2O
Tunnel Area	0.19635	Ft2
Pitot Correction	0.9290	factor
Baro. Pressure	27.93	
Pitot Factor	0.99	( 0.99 for standard, 0.84 or Cal. For S-Type )
Initial Velocity	14.166	Ft/ Sec

146.45 Ft3/min

Test Engineer: 302-



### DILLUTION TUNNEL PARTICULATE CALCULATIONS EPA Method 5G-3

Project Number: G100719074
Manufacturer: Hearth N Home
Model: OEM Large
Sample ID Number: PRT1204201552-001
Test Date: 26-Apr-12

Test Run Number: 3

Intertek Equipment No.'s 19683, 19684, 19726

OAMBI E COMPONE		FILTER#	WEIGHTS			
SAMPLE COMPONET	REAGENT	OR	FINAL, mg	TARE, mg	BLANK, mg/ml	PARTICULATE, mg
FRONT FILTER CATCH	FILTER	394	716.2			0.40
REAR FILTER CATCH	FILTER	400	164			-0.30
RINSE OF PROBE &	ACETONE	35	107606.5			
RINSE OF IMPINGER SET	WATER	205	98800.4	98797.8		2.60
RINSE OF IMPINGER SET	METHANE	100	94732.9	94733.8	0.002	0.00
RINSE OF FILTER ASSEMBLY & GAS TRAIN -	ACETONE	50	105069.3	105066.9	0.0005	
					TOTAL:	5.46

### CONDENSED WATER

	WEIGHTS			
IMPINGERS	FINAL, g	INITIAL, g	NET, g	
1	715.4	708.9	6.50	
2	697	695.5	1.50	
3	608.5	606.4	2.10	
4	1000.1	991.4	8.70	
		TOTAL:	18.80	

### **EQUATIONS**

FRONT FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
REAR FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
RINSE OF PROBE & FILTER ASSEMBLY - FRONT	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF IMPINGER SET	(Final, mg Tare, mg) (Dlank, mg/ml x Volume, mi) = Particulate, mg
RINSE OF FILTER ASSEMBLY & GAS TRAIN - BACK	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
TRINGE OF FIETER AGGEMBLE & GAG TRAIN - DACK	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg

Test Engineer:



### Supplemental Data EPA 5G/5H

Client: Hearth N Home

Model: OFML Project #: G100719074 Sample ID #: PRT 1201201 552-001

Date: 4/26//2

Run#: \_3\_

Start Time: 6904 Stop Time: 11:64

Intertek Equipment #'s: ETCS-4, ETC-11, ETC7-1

Gas Analyzer Train Leak Check:

Stack:

Calibrations:

Dilution Tunnel (Method 5G Only):

Initial: good

Initial: MA Final: \_\_\_\_

CO2: 9.96 O2: NA CO: 978 CO2(DT): NA

	N <sub>2</sub> Sp	oan	N <sub>2</sub>	Span	N₂ Span	N₂ Span	N <sub>2</sub> Span	N₂ Span	N₂ Span
Time	D	)	E	or					
O <sub>2</sub>									
CO <sub>2</sub>	-0.10	9.98	6.02	10.08	,				
СО				0.98					/
CO <sub>2</sub> (DT)									

Stack Diameter (inches): 3 h 6 "

Air Velocity (ft/min): Initial: <u>∠ 50</u>

Final: <u>450</u>

Scale Audit (lbs): Pretest:  $\underline{lOO}$  Post Test:  $\underline{lOO}$  Induced Draft:  $\underline{OO}$  %Smoke Capture:  $\underline{lOO}$ 

Pitot Tube Leak Test: Pre: OO Post: OO

Flue Pipe Cleaned Prior to First Test in Series: Date: 4/25/12

Initials: 🕰

	Initial	Middle	Ending
Pb (in/Hg)	27.95		27.91
Room Temp (°F)	7-1		7.3

Date: <u>7-1-12</u> Engineer signature: 3



Twin Ports Testing, Inc. 1301 North 3rd Street Superior, WI 54880

715-392-7114 800-373-2562

715-392-7163 www.twinportstesting.com

Report No: **Analytical Test Report** Issue No:

USR:W212-0482-01

This report replaces all previous issues

Client:

**HEARTH & HOME TECHNOLOGIES** 

1915 W Saunders St

Mount Pleasant

Attention:

Colin McCormick

PO No:

52641

Date of Issue: 4/26/2012

THIS DOCUMENT SHALL NOT BE REPRODUCED EXCEPT IN FULL

Sample Details

Sample Log No: Sample Designation: W212-0482-01

Gallon sized pellet sample

IA

Sample Recognized As: Pellets Sample Date: Sample Time:

Signed:

Arrival Date:

4/16/2012

amanda Saylıs

Amanda Sayles

Chemistry Lab Technician

Test Results MOISTURE AS UNITS **METHOD RECEIVED FREE Moisture Total** ASTM E871 wt. % 6.48 Ash **ASTM D1102** wt. % 0.26 0.24 Volatile Matter **ASTM D3175** wt. % Fixed Carbon by Difference **ASTM D3175** wt. % ulfur **ASTM D4239** wt. % 0.030 0.028 ತ೦₂ Calculated lb/mmbtu 0.065 Net Cal. Value at Const. Pressure ISO 1928 GJ/tonne 19.24 17.84 Net Cal. Value at Const. Pressure ISO 1928 19243 17839 J/g Gross Cal. Value at Const. Vol. ASTM E711 J/g 20581 19190 Gross Cal. Value at Const. Vol. ASTM E711 Btu/lb 8849 8251 Carbon **ASTM D5373** wt. % 50.33 46.93 Hydrogen **ASTM D5373** wt. % 6.15 5.73 Nitrogen **ASTM D5373** wt. % 0.20 < < 0.19 Oxygen **ASTM D3176** wt. % 43.04 40.41 Chlorine **ASTM D6721** mg/kg Fluorine **ASTM D3761** mg/kg Mercury mg/kg **ASTM D6722 Bulk Density** ASTM E873 lbs/ft3 Fines (Less than 1/8") TPT CH-P-06 wt.% **Durability Index** PDI Kansas State Sample Above 1.50" TPT CH-P-06 wt.% Maximum Length (Single Pellet) TPT CH-P-06 inch Diameter, Range TPT CH-P-05 inch to Diameter, Average TPT CH-P-05 inch Stated Bag Weight TPT CH-P-01 lbs Actual Bag Weight TPT CH-P-01 lbs

omments.



### **TEST RESULTS EPA METHOD 5G-3**

Project Number: G100719074 Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 4

Dry Burn	-Rate, kg/hr:	1.36
Emissio	n-Rate, g/hr:	0.60
Duration of Test, Minutes	12	0
Ory Gas Meter Standardization	Train A	
Dry Gas Meter Beginning Reading, ft <sup>3</sup> Dry Gas Meter Ending Reading, ft <sup>3</sup>	498.9 565.508	
Barometric Pressure Correction Factor Dry Gas Meter Calibration Factors (γ factors) Dry Gas Meter Temperature Factors Dry Gas Meter Delta-H Correction Factors	0.937 0.994 0.990 1.002	
Dry Gas Meter STD Volume Sampled, ft <sup>3</sup>	61.562	
Dillution Tunnel Flow / Volume		
Standardized Tunnel Flow, dscfm	126.	
Total Tunnel Volume, scf	15160	.211
mission Caclulations	Train A	
Sample Ratios (Total Tunnel Volume / Total Sample Volume) Sample Particulate Mass, mg Total Emissions, grams	246.260 4.9 1.195	
Emission-Rate, g/hr Adjusted Emission Rates, g/hr	0.60 <b>1.19</b>	
Operating Parameters	Train A	
Max Filter Temperature, °F Post-Test Leak Check, cfm @ in. Hg vac.	235 0.0 @ 5	
Average Firebox Surface Temperture delta-T, °F Maximum Ambient Temperture, °F Mimimum Ambient Temperature, °F	21. 76 71	3
uel Properties		
Wet Fuel Load Weight, lb. Dry-Basis Fuel Load Moisture Content, % Wet-Basis Fuel Load Moisture Content, %	6.4 6.0 6.0	8

Test Engineer: BOD

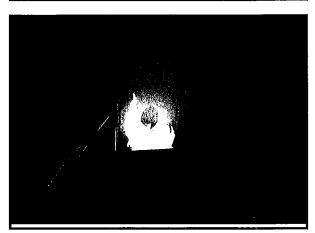


### Run Notes EPA Methods 28 and 5G-3

PROJECT / TEST INFORMATION					
Project Number:	G100719074				
Manufacturer:	Hearth N Home				
	OEM Large				
Sample ID Number:	PRT1204201552-001				
Test Date:	26-Apr-12				
Test Run Number:	4				
Date tunnel cleaned:	4/25/2012				
Purpose of Test	Certification				

Applia	nce Inform	ation
Appliance Type:	3	1 - Catalytic 2 - Non - Catalytic 3 - Pellet 4 - Hydronic
Firebox Volume, ft <sup>3</sup> :	0	N/A for pellet type
Convection Blower	3	1 - No Fan 2 - Fan Optional 3 - Fan Standard





		Test Settings
	Primary Air:	
	econdary Air:	
C		Set at medium high via a computor interface
	Blower/Fan:	
		Pre- Burn Activities
Time	Activity	
	No activity w	as noted
		Start-Up Procedure
	of fuel, sec. :	
Fuel-I	oading door :	
	Primary air:	
	econdary air:	
	Control board:	Computer input to hold constant burn rate
	Blower / fan:	
		Other Notes
2200 rpm	on combustio	n blower, 2.2 seconds on time out of a 7 second duty cycle.

Test Engineer: 300\_\_\_

Date: 3-1-12



## TEST FUEL DATA EPA METHOD 5G-3

Project Number: G100719074

Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 4

Firebox	Volume, ft <sup>3</sup> :	0	

Calibration Reference ID			
Set meter to Species 1			
Set Temperature to 70F	12%	12.0	
Set pin setting to 444	22%	22.0	

	PRE-BURN FUEL PROPERTIES								
Eq. ID No.:		Time:	Temp.,°F:						
Piece No.	Length, In.	Weight, Lb.	Moisture, %, Dry Basis						
1									
_ 2									
3									
4									
5									
6									
7									
8									
9									
10									
11									
12									
Total We	eight	0.0	Average, %db	#DIV/0!					

Allowable Fuel Load Range: 0.0 to 0.0

	TEST FUEL LOAD PROPERTIES							
Eq. ID No.:			Time:		Temp.,°F:			
Piece No.	Length,	Weigl	ht, Lb.	Moio	ture, %, Dry E	Pooio		
Tiece No.	ln.	2x4	4x4	IVIOIS	ture, 70, Dry c	วสรเร		
1		6.40		6.5	6.5	6.5		
2								
3								
4								
5								
6								
7								
8								
Total	S	6.4	0.0					
% of We	eight	100	. 0					
Total weight	, wet, lb.	6.	40	Average Moisture, dry 6.48		6.48		
Total weight	, dry, kg	2.	73	Average Moisture, wet		6.09		

Test Engineer:



Project Number: G100719074

Manufacturer: Hearth N Home

OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 4

### EPA Method 28 Pre Burn Data

Coal Bed Range 1.3 to 1.6

Average Firebox Temp, °F 465.2

Final Coal Bed Wt, lb 51.4

	Temperature Data											
Duration, Minutes	Room	Dilution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Flue Draft	Fuel Weight	Weight Loss
0	74	86	224	498	464	380	479	456		-0.032	54.60	3.20
10	75	88	223	512	458	373	484	459		-0.033	54.00	0.60
20	73	87	222	509	459	374	477	455		-0.033	53.50	0.50
30	74	88	226	485	442	366	465	441		-0.033	53.00	0.50
40	74	88	224	517	455	378	485	441		-0.033	52.50	0.50
50	74	87	222	520	463	380	484	460		-0.032	51.90	0.60
60	73	86	225	515	468	386	490	467		-0.032	51.40	0.50
										_		
										•		

Test Engineer: 0500



Project Number: G100719074

Manufacturer: Hearth N Home

Model: OEM Large

Sample ID No: PRT1204201552-001

Test Date: 26-Apr-12

Test Run No: 4

**Temperature Data** 

Firebox Temp Start 466.2
Firebox Temp End 445
Firebox Delta-T 21.2

Max Filter Temps							
Train A							
235							

Interval	10	Dura	tion of Tes	t, Min	120									
Ī	ime						Te	mperature	Data					
Interval	Duration	Room	Dillution Tunnel	Flue Gas	Firebox Top	Firebox Bottom	Firebox Back	Firebox Left	Firebox Right	Catalyst Outlet	Train A Filter	lmpinger Exit	Train A DGM	
0	0	76	88	225	522	466	387	491	465		235	76	74	
1	10	76	88	226	537	468	391	501	473		234	54	74	
2	20	73	87	225	519	466	382	487	461		233	53	74	
3	30	73	86	221	484	436	358	459	433		234	54	74	
4	40	73	86	222	499	453	373	479	448		234	54	74	
5	50	72	86	221	499	450	371	474	445		234	54	73	
6	60	71	86	224	528	457	384	493	462		235	54	73	
7	70	72	86	226	524	464	387	496	466		233	54	73	
8	80	74	87	225	500	457	380	485	455		234	55	73	
9	90	74	87	222	503	433	361	472	440		234	56	73	
10	100	75	86	223	524	449	378	491	459		233	56	73	
11	110	73	86	223	500	458	374	478	449		235	57	73	
12	120	73	86	223	494	447	366	473	445		233	59	73	

Test Engineer: BD -



### **Gas Particulate Sampling Data**

0.994

Project Number: G100719074

Manufacturer: Hearth N Home Model: OEM Large

Sample ID Number: PRT1204201552-001

Barometer, In. Hg RH, % Sample Box Correction (y) Factors

Meter Box (A)

Test Date: 26-Apr-12

Start 27.91

28.16

End

Test Run Number: 4

Le	eak Check	cfm @ in Hg
	Train A	
	0.0 @ 5	

Maximum Vacuum							
Train A							
0.00							

Durat	ion of Test	, Min	120						
		Particulate Sampling Data							
1								Train A	Train A
ŀ	Tunnel	Train A		Flue	Fuel	Weight	Train A	Proportional	Vacuum, In.
Time	Delta-P	Delta-H		Draft	Weight	Loss	Volume	Rate	Hg
0	0.034	1.00		-0.032	51.30	6.40	498.900	99.99	0.00
10	0.034	1.00		-0.032	50.70	0.60	504.690	104.32	0.00
20	0.034	1.00		-0.032	50.20	0.50	510.020	95.95	0.00
30	0.034	1.00		-0.032	49.70	0.50	515.580	99.99	0.00
40	0.034	1.00		-0.032	49.10	0.60	521.350	103.77	0.00
50	0.034	1.00		-0.032	48.60	0.50	527.010	101.98	0.00
60	0.034	1.00		-0.032	48.10	0.50	532.630	101.26	0.00
70	0.034	1.00		-0.032	47.50	0.60	537.950	95.86	0.00
80	0.034	1.00		-0.032	47.00	0.50	543.380	97.93	0.00
90	0.034	1.00		-0.032	46.50	0.50	548.840	98.47	0.00
100	0.034	1.00		-0.032	46.00	0.50	554.300	98.38	0.00
110	0.034	1.00		-0.032	45.40	0.60	559.930	101.44	0.00
120	0.034	1.00		-0.032	44.90	0.50	565.508	100.51	0.00

Test Engineer: B



# Dillution Tunnel Velocity Traverse EPA Method 5G-3

Project Number: G100719074 Manufacturer: Hearth N Home

Model: OEM Large

Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12

Test Run Number: 4

	Dilution	Tunnel	
	Delta P In. H2O	Temp,°F	Square Root
A1	0.0260	87	0.1612
A2	0.0320	87	0.1789
A3	0.0360	87	0.1897
A4	0.0300	87	0.1732
A Center	0.0340	87	0.1844
B1	0.0260	87	0.1612
B2	0.0320	87	0.1789
B3	0.0360	87	0.1897
B4	0.0320	87	0.1789
B Center	0.0340	87	0.1844
Averages	0.0318	87	0.1765

Tunnel Diameter	6.000	inches
Tunnel Static	-0.300	in. H2O
Tunnel Area	0.19635	Ft2
Pitot Correction	0.9571	factor
Baro. Pressure	27.91	
Pitot Factor	0.99	( 0.99 for standard, 0.84 or Cal. For S-Type )
Initial Velocity	12.378	Ft/ Sec
Initial Flow	126.00	Ft3/min

Test Engineer: 8

Date: 7-/-/2



### DILLUTION TUNNEL PARTICULATE CALCULATIONS EPA Method 5G-3

Project Number: G100719074
Manufacturer: Hearth N Home
Model: OEM Large
Sample ID Number: PRT1204201552-001

Test Date: 26-Apr-12
Test Run Number: 4

Intertek Equipment No.'s 19683, 19684, 19726

		FILTER #	WEIGHTS			
SAMPLE COMPONET	REAGENT	OR	FINAL, mg	TARE, mg	BLANK, mg/ml	PARTICULATE, mg
FRONT FILTER CATCH	FILTER	395	715.9		STATE AND ADDRESS.	2.00
REAR FILTER CATCH	FILTER	405	165.2	165.7		-0.50
RINSE OF PROBE &	ACETONE	40	108637.3	108637.4	0.0005	-0.12
RINSE OF IMPINGER SET	WATER	200	107982.6	107980.9	0	1.70
RINSE OF IMPINGER SET	METHANE	100	108416.4	108416.4	0.002	0.00
RINSE OF FILTER ASSEMBLY & GAS TRAIN -	ACETONE	55	110222.6	110220.8	0.0005	1.77
					TOTAL:	4.85

### CONDENSED WATER

	WEIGHTS						
IMPINGERS	FINAL, g	INITIAL, g	NET, g				
1	717.1	710.9	6.20				
2	695.7	690.8	4.90				
3	607.7	607.4	0.30				
4	985.6	970	15.60				
		TOTAL:	27.00				

### **EQUATIONS**

Edertifotto	
FRONT FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
REAR FILTER CATCH	Final, mg - Tare, mg = Particulate, mg
RINSE OF PROBE & FILTER ASSEMBLY - FRONT	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF IMPINGER SET	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg
RINSE OF FILTER ASSEMBLY & GAS TRAIN - BACK	(Final, mg - Tare, mg) - (Blank, mg/ml x Volume, ml) = Particulate, mg

Test Engineer:



## Supplemental Data EPA 5G/5H

Client: Hearth N Home

Model: DEM L Project #: G100719074 Sample ID #: PRT 1201201552-001

Run #: \_\_\_\_\_\_\_

Start Time: 12.54

Stop Time: 14:59

Intertek Equipment #'s: ETCS-Y, Frc-", Frc7-1

Gas Analyzer Train Leak Check:

Stack:

Calibrations:

Dilution Tunnel (Method 5G Only):

Initial: gard
Final: good
Span Gas

Initial: M

	N₂ Span		N₂ Span		N <sub>2</sub> Span	N <sub>2</sub> Span	N₂ Span	N <sub>2</sub> Span	N <sub>2</sub> Span
Time							_		
O <sub>2</sub>									
CO <sub>2</sub>	0.02	10.08	- 0.06	10.00					
СО	0.00	0.98	0.00	0.97					
CO <sub>2</sub> (DT)	WA			•					

Stack Diameter (inches): 3 / 6 "

Air Velocity (ft/min): Initial: <u>~50</u> Final: <u>~50</u>

Scale Audit (lbs): Pretest: 100 Post Test: 101

Induced Draft: 0.0 %Smoke Capture: 100%

Pitot Tube Leak Test: Pre: O.U Post: O.U

Flue Pipe Cleaned Prior to First Test in Series: Date:  $\frac{c\sqrt{15}/(2)}{2}$ 

Initials: <u>パン</u>

	Initial	Middle	Ending
Pb (in/Hg)	2791		28.16
Room Temp (°F)	76		73

Date: 7-1-12

Engineer signature: 3



Twin Ports Testing, Inc. 1301 North 3rd Street Superior, WI 54880

715-392-7114 800-373-2562

Report No:

Issue No:

715-392-7163 www.twinportstesting.com

This report replaces all previous issues

## **Analytical Test Report**

52641

1915 W Saunders St

Mount Pleasant

Colin McCormick

Attention:

PO No:

Client:

Signed:

amanda Saylıs

Amanda Sayles

Chemistry Lab Technician

USR:W212-0482-01

Date of Issue:

4/26/2012

THIS DOCUMENT SHALL NOT BE REPRODUCED EXCEPT IN FULL

Sample Details

Sample Log No:

Sample Designation:

W212-0482-01

**HEARTH & HOME TECHNOLOGIES** 

Gallon sized pellet sample

Sample Recognized As: Pellets Sample Date: Sample Time:

**Arrival Date:** 

4/16/2012

Test Results				articore de la crista de la final de la crista que escuela de la crista de la crista de la crista de la crista
			MOISTURE	AS
	METHOD	UNITS	FREE	RECEIVED
Moisture Total	ASTM E871	wt. %		6.48
Ash	ASTM D1102	wt. %	0.26	0.24
Volatile Matter	ASTM D3175	wt. %		
Fixed Carbon by Difference	ASTM D3175	wt. %		
lfur	ASTM D4239	wt. %	0.030	0.028
JO₂	Calculated	lb/mmbtu		0.065
Net Cal. Value at Const. Pressure	ISO 1928	GJ/tonne	19.24	17.84
Net Cal. Value at Const. Pressure	ISO 1928	J/g	19243	17839
Gross Cal. Value at Const. Vol.	ASTM E711	J/g	20581	19190
Gross Cal. Value at Const. Vol.	ASTM E711	Btu/lb	8849	8251
Carbon	ASTM D5373	· wt. %	50.33	46.93
Hydrogen	ASTM D5373	wt. %	6.15	5.73
Nitrogen	ASTM D5373	wt. %	< 0.20	< 0.19
Охудеп	ASTM D3176	wt. %	> 43.04	> 40.41
				-
Chlorine	ASTM D6721	mg/kg		
Fluorine	ASTM D3761	mg/kg		
Mercury	ASTM D6722	mg/kg	Mark	
Bulk Density	ASTM E873	3		
Fines (Less than 1/8")	TPT CH-P-06	lbs/ft <sup>3</sup> wt.%		
Durability Index	Kansas State	wt.% PDI		
Sample Above 1.50"	TPT CH-P-06	wt.%		
Maximum Length (Single Pellet)	TPT CH-P-06			
Diameter, Range	TPT CH-P-05	inch		4.0
Diameter, Average	TPT CH-P-05	inch inch		to
Stated Bag Weight	TPT CH-P-05	lbs		
Actual Bag Weight	TPT CH-P-01	lbs		
Actual Day Weight	1F1 Un-r-01	RUS		
Annia			****	

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